

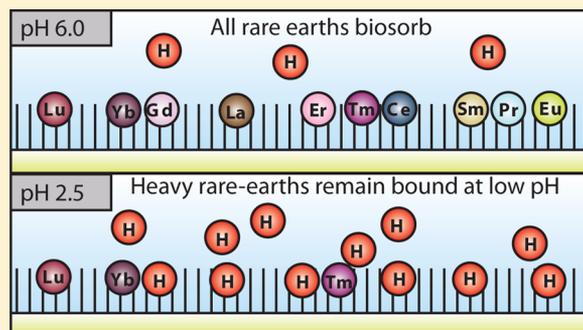
## Rare-Earth Separation Using Bacteria

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**S** Supporting Information

**ABSTRACT:** The rare-earth elements are critical to many green energy technologies but are difficult to separate from one another because of their chemical similarity. We demonstrate an alternative, biogenic method based on the adsorption of lanthanide to the bacterium *Roseobacter* sp. AzwK-3b, immobilized on an assay filter, followed by subsequent desorption as a function of pH. The elution desorption data suggest that the basicity of the individual lanthanides is important in determining their desorption behavior. It is found that via preprotonation of the bacteria it is possible to concentrate a solution of equal concentrations of each lanthanide to nearly 50% of the three heaviest lanthanides (Tm, Lu, and Yb) in just two passes. This surpasses existing industrial practice. The findings suggest that there is an opportunity to harness the diversity of bacterial surface chemistry to separate and recover technologically important rare-earth metals in an environmentally benign manner.



### INTRODUCTION

It is widely recognized that the rare-earth lanthanide elements (La through Lu) are crucial constituents in advanced materials for many existing and future energy technologies.<sup>1</sup> The rare earths, notably Dy, Nd, and Sm, are used, for instance, in high-energy density permanent magnets in electric motors and generators such as those in electric vehicles and wind turbines.<sup>2,3</sup> Eu and Tb are used in phosphors for solid state lighting,<sup>4</sup> and La and Ce, for instance, are used as anode materials in nickel metal hydride batteries. Unfortunately, because the lanthanides are chemically similar, are trivalent, and have similar ionic radii, they are difficult to separate from one another by physical or chemical means. The dependence of many green energy technologies on the lanthanides, coupled with the challenges associated with their extraction and recovery, led the U.S. Department of Energy to classify six of the lanthanides as either critical or near-critical elements.<sup>5</sup> This criticality as well as the search for more environmentally benign processing motivates the need for new methods of lanthanide separation and recovery, including in recycling. In this work, an alternative approach based on microbial biosorption and desorption as a function of pH is described.

The standard industrial method of separating lanthanides, after ore processing,<sup>6</sup> to produce an aqueous mixture of the lanthanides, usually as chlorides, uses solvent extraction. In this process, the solution is combined with an immiscible organic liquid such as EHEHPA (2-ethylhexyl phosphonic acid mono-2-ethylhexyl ester).<sup>6</sup> The lanthanide ions partition between the organic and aqueous phases on the basis of their basicity. In turn, these differences produce different solubilities in the two liquid phases. Then, the aqueous and organic liquids are isolated, and the lanthanides are recovered from each.

To increase the concentration of the recovered elements, the enriched solutions are continuously fed through numerous solvent extraction stages until the desired purity is reached.<sup>6</sup>

Until now, biosorption of metals to bacteria has primarily been of interest for the remediation of toxic elements, such as As, Pb, and Cd, from wastewater as well as to limit the release of metals from mine drainage streams. These environmentally important applications have motivated extensive studies of biosorption of toxic elements and more common metals, such as Cu, Zn, and Ni, as well as the underlying binding mechanisms.<sup>7–9</sup> Recently, however, a limited but convincing literature has shown that a number of individual lanthanides can biosorb to bacterial surfaces.<sup>10–16</sup>

In this work, we show that all the lanthanides biosorb from a mixed lanthanide solution and can then be separated under semicontinuous flow conditions with decreasing pH washes. Via systematic variation of the wash pH after biosorption, different lanthanides from a mixed lanthanide solution can be separated by preferentially desorbing them from the bacterial surface. We illustrate this using *Roseobacter* sp. AzwK-3b, a Gram-negative marine bacterial strain whose genus has been shown to be a strong metal absorber.<sup>17</sup>

### MATERIALS AND METHODS

**Media and Reagents.** A mixed lanthanide solution (Accutrace, New Haven, CT), a calibration standard for ICP-MS, was used as the base solution for all the work reported here.

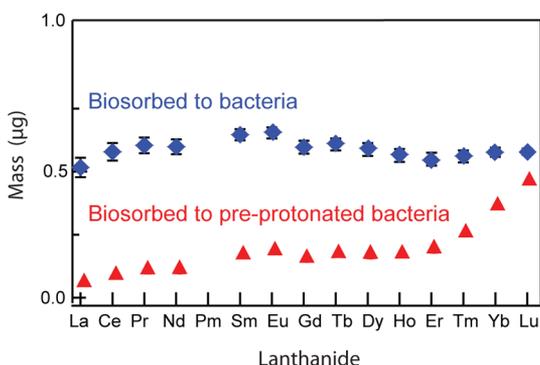
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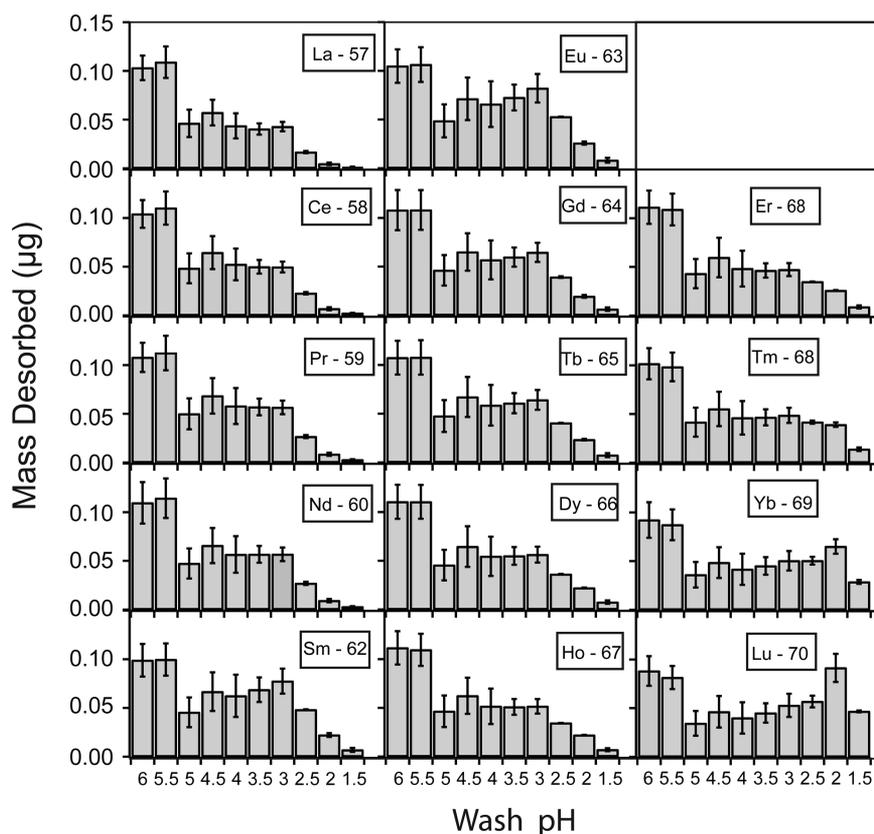
It contains each lanthanide (except Pm) at a concentration of 10  $\mu\text{g}/\text{mL}$ , as well as Sc, Y, and Th, all dissolved in 2% nitric acid. For all the assays, this solution was first diluted with deionized water and neutralized to pH 6.0 to a concentration of 2  $\mu\text{g}/\text{mL}$ .



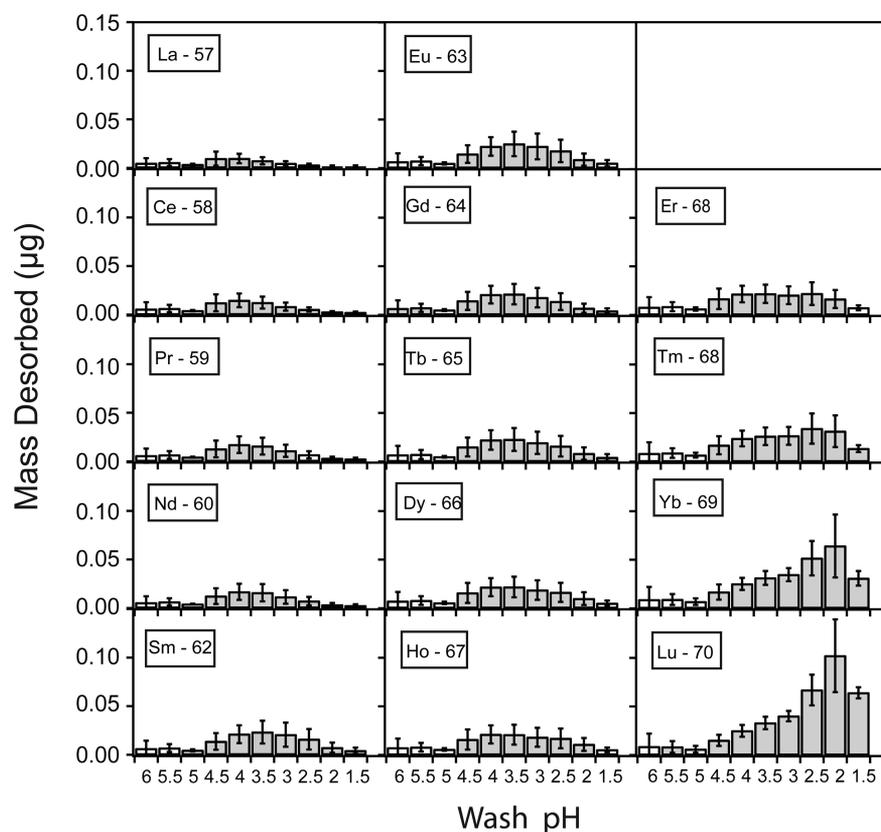
**Figure 1.** Mass of each lanthanide adsorbed to *Roseobacter* sp. AzwK-3b from an equi-mass 1 mL solution of all the rare earths during the filtration assay. Biosorption was almost independent of the lanthanide atomic number, although there is a slight preference for the middle lanthanides. The mass of the lanthanides adsorbed to the bacterial surface after first protonating the surface at pH 2.5 is also shown. There is reduced biosorption of the lighter rare earths but similar biosorption of the heavier rare earths compared to biosorption before protonation (repeated in triplicate). The error bars are commensurate with the symbol size.

*Roseobacter* sp. AzwK-3b is a bacterial strain from Elkhorn Slough, a coastal estuary close to Monterey Bay, CA.<sup>18</sup> It was grown in artificial seawater (ASW) first sterilized by being autoclaved at 120 °C for 15 min. A single stock of *Roseobacter* sp. AzwK-3b was created by inoculating 1 L of sterile ASW with *Roseobacter* sp. AzwK-3b and allowing it to incubate at 37 °C for approximately 2 months. The biomass was kept refrigerated and sterilely removed from this stock as wet biomass for all the experiments. When the bacteria had dried, their mass was found to be 0.05 mg/mL of medium.

**Continuous Flow Filtration Assay.** The assay was developed to quantify lanthanide biosorption as well as to expose the bacteria and biosorbed lanthanides to various pH washes; 2 mL of the bacterial medium (~0.1 mg) was immobilized on a 25 mm diameter hydrophilic, polypropylene filter (Pall, Port Washington, NY; GHP Acrodisc), and a syringe pump was used to pass solutions over the bacteria. The filter was selected because its average pore size (0.2  $\mu\text{m}$ ) was smaller than the diameter of the bacteria (0.8  $\mu\text{m}$ ). As described in the [Supporting Information](#), a constant, optimized flow rate of 2.5 mL/min was used for all the assays, and it was demonstrated that no biosorption occurred on the filter absent the bacteria. The biosorption step consisted of passing 1 mL of the mixed lanthanide solution through the filter. This was followed by a 5 mL deionized water wash (pH 7) to remove any lanthanides not bound to the bacteria. For the desorption, a series of 5 mL nitric acid solutions, from pH 6 to 1.5, in



**Figure 2.** Mass of individual lanthanides desorbed from *Roseobacter* sp. AzwK-3b at 0.5 pH unit intervals as a function of pH washes of each 5 mL volume. Although the masses of the lanthanides desorbed during the two highest-pH washes, pH 6 and 5.5, were relatively insensitive to atomic number, lower-pH washes revealed marked differences with atomic number. Furthermore, the graphs indicate more light lanthanides desorbed with higher-pH washes and more heavy lanthanides desorbed with lower-pH washes. Local maxima in the mass desorbed with successively lower pH suggest there may be as many as three distinct bacterial sites, corresponding to pH's of 5.5–6.0, 4.5–3.0, and 2.5, that are responsible for lanthanide absorption. The error bars represent the standard deviation of at least three replicates.



**Figure 3.** Effect of first preprotonating the *Roseobacter* sp. AzwK-3b with 5 mL of a pH 2.5 nitric acid wash on the mass of each lanthanide desorbed during subsequent titration as a function of pH. The bacteria desorbed smaller amounts of all the lanthanides at washes with pH's higher than that of the preprotonation wash (pH 2.5) as compared to that shown in Figure 2. Similar masses of the lanthanides desorbed at washes with pH's lower than the preprotonation pH. As shown, these were enriched with the heaviest lanthanides. Same mass scale as Figure 2. The error bars represent the standard deviation of at least three replicates.

intervals of 0.5 pH unit, was successively pumped past the bacteria on the filter.

**ICP-MS.** The masses of the lanthanides absorbed and desorbed were determined by ICP-MS of their concentrations in 5 mL aliquots.

**Preprotonation.** The bacterial surface was preprotonated in the same apparatus using 5 mL solutions of pH 2.5 nitric acid.

**Lanthanide Separation.** The same flow method was used but with additional passes (stages) over fresh bacteria preprotonated with different pH washes as described in the flow diagram in Figure S2 of the Supporting Information.

## RESULTS AND DISCUSSION

The biosorption of the individual lanthanides to the *Roseobacter* sp. AzwK-3b bacteria from equi-concentration lanthanide solutions at pH 7 is shown in Figure 1. The bacteria strongly absorbed each lanthanide with a slight statistical preference for the middle lanthanides. The total biosorption was found to vary from one batch of bacteria to another. We attributed this to variations in the effective bacterial surface area exposed to the fluid flow in the assays resulting from variations in the local density of the bacteria immobilized on the filter. Despite this, the relative values within the lanthanide series of each biosorption run were consistent.

After adsorption, the bacteria were washed at successively decreasing pH's. The mass of each lanthanide desorbed is shown in Figure 2. The data indicate that a larger fraction of the

lighter lanthanides desorbed with the highest-pH washes, while the reverse is true for the lowest-pH washes. Moreover, comparison of the masses desorbed indicates that the heaviest lanthanides, in particular Tm, Yb, and Lu, were preferentially desorbed at the lowest pH's. Comparison of the data for the heaviest, and smallest, lanthanide, Lu, with the lightest and largest lanthanide ion, La, indicates that the mass of Lu desorbed at the lowest pH was 25-fold greater than that of La. The variation was quantified by a desorption ratio,  $R_{AB}$ , the ratio of the desorbed masses of two different lanthanides, A and B, at the same pH. The equivalent separation factor,  $\alpha_{AB}$ , used in other branches of separation chemistry,<sup>19</sup> is the ratio  $(R_{AB})_1 / (R_{AB})_2$ , where the subscripts refer to the pH at which the desorption masses are compared. For the purpose of illustration, the separation factors among four pairs of neighboring lanthanides are compared in Table S1 of the Supporting Information.

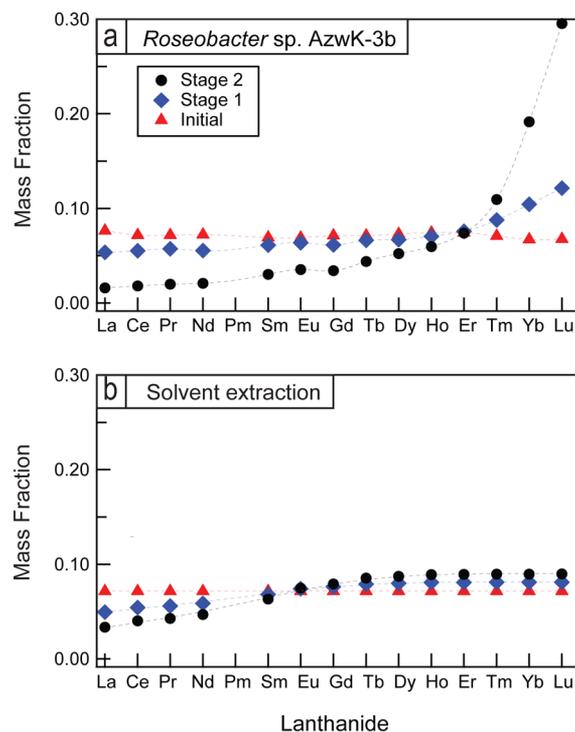
The biosorption and pH desorption results are consistent with lanthanide ions binding to, and desorbing from, sites on the bacterial surface according to their acid dissociation constants ( $pK_a$ 's). (In strict terms, the  $pK_a$  of a surface site is the pH at which 50% of the lanthanides desorb from a surface site and are replaced by protons.) Although the number of distinct surface binding sites on the *Roseobacter* sp. AzwK-3b is unknown, the desorption elutions suggest that there are, possibly, three types of sites to which lanthanide ions can absorb. These broad maxima, which occur at approximate  $pK_a$ 's of 5.5–6.0, in the range of 3.0–4.5, and of ~2.0, are quite

reproducible from run to run using *Roseobacter* sp. AzwK-3b, so there is conjecture that these correspond to the presence of possibly three distinctive types of binding sites on the bacterial surface. The results in Figure 2 indicate that surface sites having higher  $pK_a$ 's tend to bind the lighter, more basic lanthanides and those having lower  $pK_a$ 's tend to bind the heavier, more acidic lanthanides. The underlying reasons for the correlation between the observed lanthanide desorption with  $pK_a$  and the basicity of the lanthanide ion are unknown. The simplest explanation is that it is related to the well-established, systematic decrease in basicity with increasing atomic mass across lanthanide series and the associated decreasing ionic size across the series, the so-called lanthanide contraction.<sup>20,21</sup>

**Effect of Preprotonation.** Evidence of the solution pH controlling individual lanthanide desorption was sought using preprotonation experiments in which the bacteria were first washed with a highly acidic solution (pH 2.5) and then exposed to the mixed lanthanides. It would be expected that upon preprotonation, protons preferentially absorb to all the surface sites having a  $pK_a$  higher than the preprotonation pH. Then, on exposure to the lanthanide solution, there would correspondingly be lower absorption of the lanthanides to those sites preprotonated by washing at pH 2.5. Specifically, sites having lower  $pK_a$ 's would not be protonated and consequently would bind the heaviest lanthanides just as they do without preprotonation. The experimental findings are shown in Figure 3, on the same scale as the data in Figure 2. As anticipated, substantially less of each lanthanide desorbed with pH washes above the preprotonation pH, whereas similar values of the lanthanide masses were recovered using pH washes below the preprotonation pH.

**Lanthanide Separation.** The observed variation in pH at which different lanthanides preferentially desorb provides the basis for the possible use of bacteria in separating and recovering individual lanthanides from solution. While the separation factors that can be achieved in a single elution assay are significant, it is likely that multiple biosorption–desorption steps would be required to attain a desired level of enrichment just as in the current solvent extraction process. To demonstrate the efficacy of such a multiple step process in purifying the heaviest lanthanides, the continuous flow assay was repeated by passing the lanthanide solution over fresh, preprotonated bacteria (see Materials and Methods and the flow diagram in the Supporting Information for details). The results presented in Figure 4a show a progressive enrichment of the three heaviest lanthanides; after the second pass, the solution contained 18 wt % Yb and 30 wt % Lu. While the value of the preprotonation pH was specifically selected to preferentially separate the heaviest lanthanides, it was found, but not shown in this publication, that the preprotonation pH could be adjusted, to recover and cycle different washes through the assay to recover other groups of lanthanides, such as the middle lanthanides.

To illustrate the potential of the bacterial separation approach, the quantitative findings in Figure 4a can be compared to the results of the standard industrial method, using solvent extraction, of separating the lanthanides (see Figure 4b). The comparison is based on calculating the enrichment after two stages of the industrial solvent extraction method using the separation factors cited for the process.<sup>6</sup> The calculations are given in the Supporting Information. The two-pass biosorption–desorption enrichment process using



**Figure 4.** (a) Purification of the heaviest lanthanides. The mass fractions of each lanthanide initially in solution and then after the first and second passes of the same solution over freshly preprotonated bacteria illustrate concentration enrichment of the three heaviest lanthanides, Tm, Yb, and Lu. After the second pass, the solution contains 48% of the two heaviest lanthanides, Yb and Lu, exceeding the calculated enrichment performed using solvent extraction shown in panel b. After each pass, the bacteria were replaced by a new batch of bacteria and preprotonated with a pH 2.5 wash.

*Roseobacter* sp. AzwK-3b achieves purities comparable, if not superior, to those of the industrial process.

Although the results suggest that preferential binding of lanthanide ions depends on the pH, more detailed studies, for instance by EXAFS, are clearly needed to identify the functional groups responsible for binding to specific lanthanides. However, it is also possible that surface molecules, such as polysaccharides and lipids, as well as functional groups, such as carboxyl groups, can also bind to some of the lanthanides. Takahashi et al.,<sup>16</sup> for example, reported the preferential adsorption of the middle rare earths to carboxyl groups from molecules such as acetate and propionate. Similarly, there are biosorption studies<sup>10,12–14,22,23</sup> showing that the heaviest lanthanides preferentially bind to phosphate groups, which have a  $pK_a$  of  $\sim 2.0$ ,<sup>24</sup> consistent with our findings that the last lanthanides, Yb and Lu, to desorb are also the most acidic. However, it is likely that the lanthanide binding is more complicated and that there is competition not only between the protons and the lanthanide ions in solution for specific surface sites but also between different lanthanides. Furthermore, it is extremely unlikely that specific lanthanides will bind to specific sites and more likely that there is a distribution in binding energies as well as local steric effects involved. These questions clearly warrant more detailed structural biochemical characterization of lanthanide binding, but until then, the interpretation in terms of the values of  $pK_a$  seems to be useful if too simplistic.<sup>25</sup>

Although at only the laboratory scale and not optimized, our results suggest that the bacterial sorption–elution desorption

process may be more benign than current commercial solvent extraction processes. We used *Roseobacter* sp. AzwK-3b as the biosorbing material but anticipate that lanthanide separation will be achievable using other bacteria because the surface groups implicated in this work commonly occur on the surfaces of other bacteria and are not expected to be unique to *Roseobacter* sp. AzwK-3b. Indeed, similar results but differing in the numerical values of separation factors have been obtained with three other bacteria, *Shewanella oneidensis*, *Sphingobacterium* sp., and *Halomonas* sp. An example is shown in Figure S3 of the Supporting Information for lanthanide desorption from *S. oneidensis*, another bacterium known to be a metal absorber. Given the rich variety of bacterial surface chemistries, it is also likely that other bacteria will exhibit significantly greater differentiation in binding different lanthanides. It is also possible that other metals can be separated from one another using similar absorption–desorption elution methods. This may also be important in separating specific heavy metals after bioremediation.

## ■ ASSOCIATED CONTENT

### 📄 Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acs.estlett.6b00064.

Additional methods, calculations, and figures, as referenced in the text (PDF)

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### Notes

The authors declare no competing financial interest.

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